

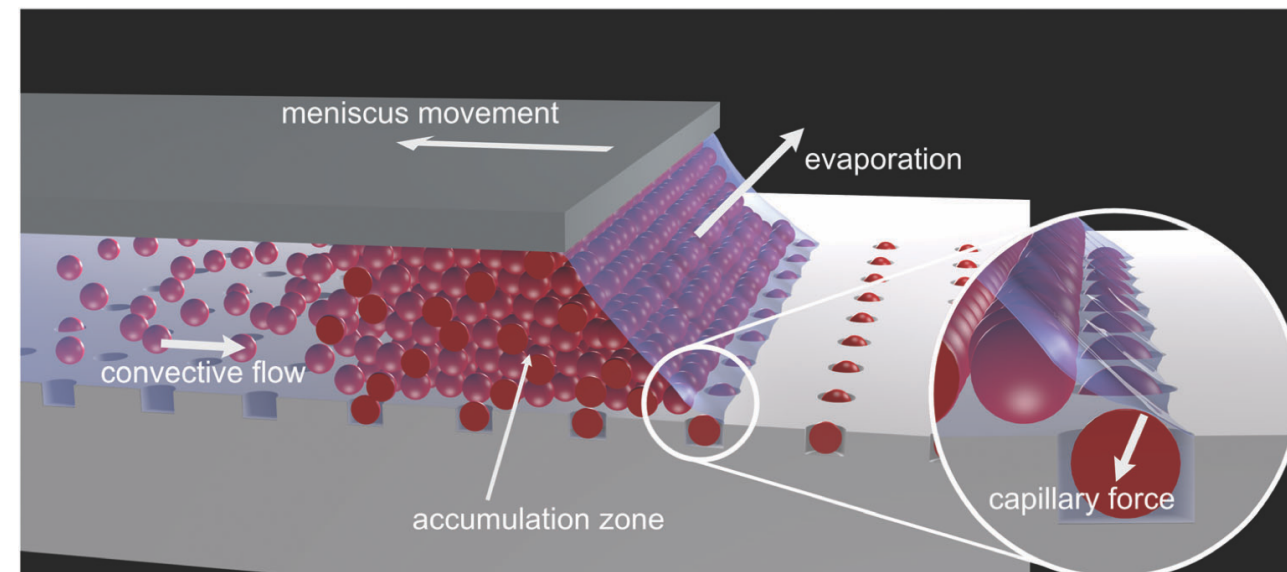
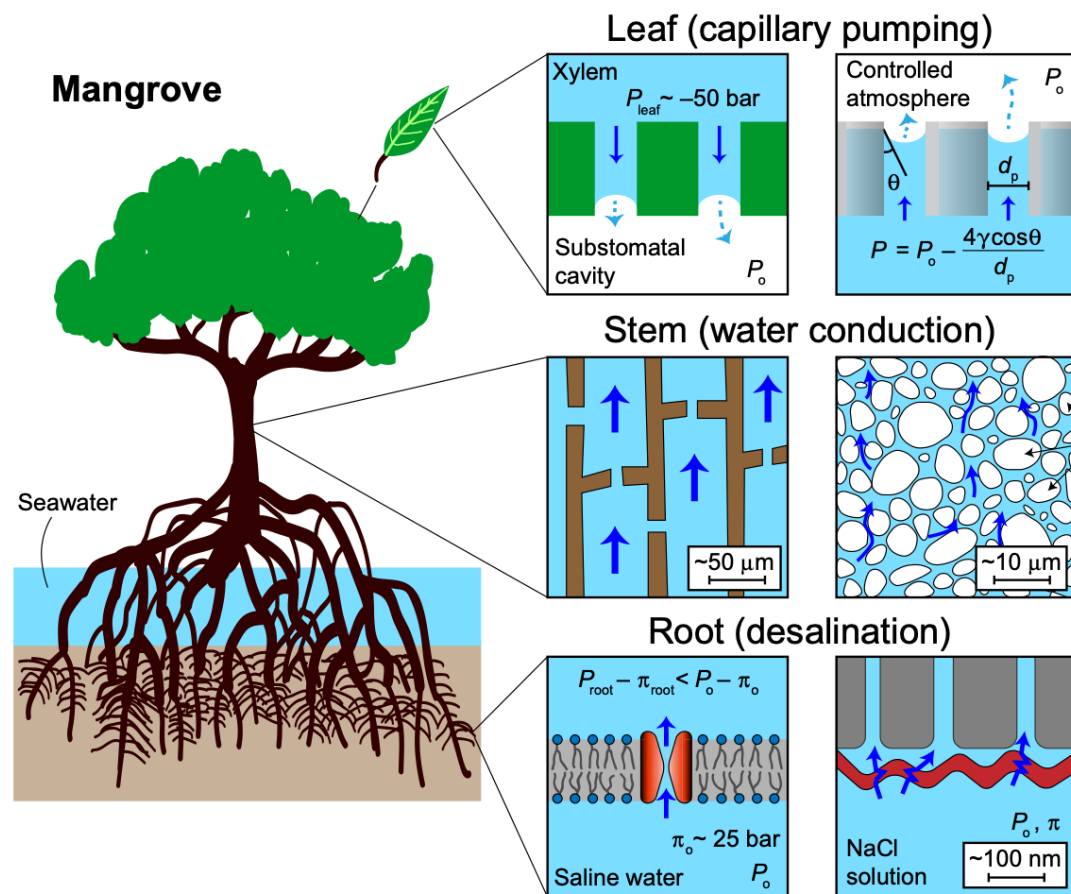
ChE-402: Diffusion and Mass Transfer

Lecture 4

Intended Learning Outcome

- ✦ To solve steady-state problems involving both convection and diffusion.
- ✦ To further analyze the link between velocity, diffusion, and convection.

Capillary evaporation



SCIENCE ADVANCES | RESEARCH ARTICLE

ENGINEERING

Capillary-driven desalination in a synthetic mangrove

Yunkun Wang^{1,2}, Jongho Lee^{2,3}, Jay R. Werber^{2,4}, Menachem Elimelech^{2*}

Soft Matter

REVIEW



View Article Online
View Journal | View Issue

Capillary assembly as a tool for the heterogeneous integration of micro- and nanoscale objects

Songbo Ni, ^{ab} Lucio Isa ^{*b} and Heiko Wolf ^{id *a}

Solving the evaporation problem in stagnant air

Calculate flux and concentration profile of evaporating benzene in stagnant air.

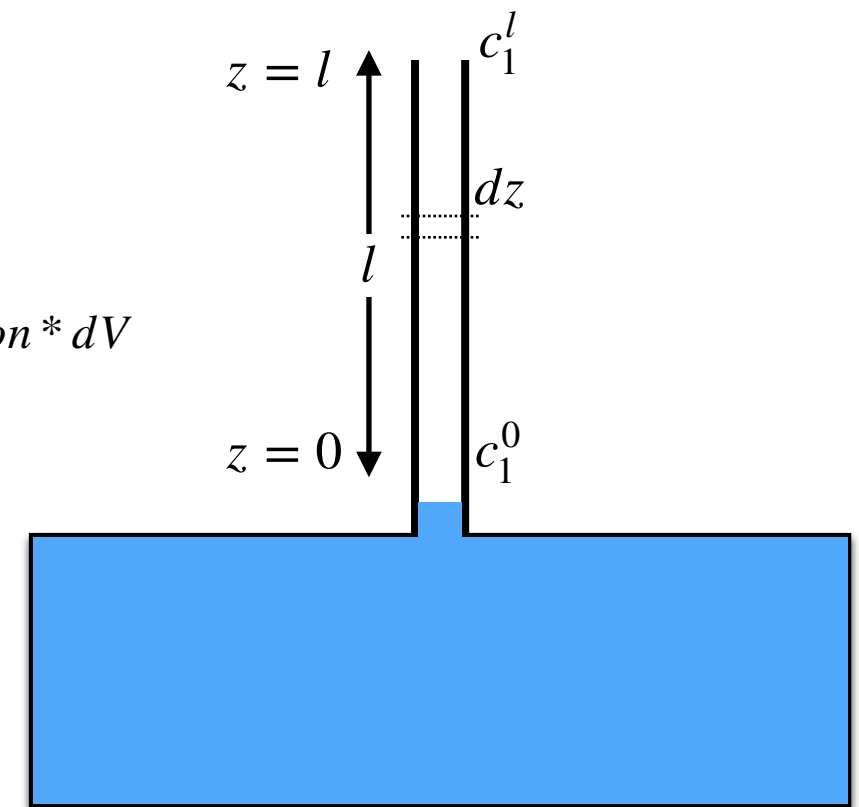
By stagnant air, we are approximating the velocity of air to be zero (total flux of air $n_2 = c_2 v_2 = 0$).

Define your system - capillary tube

Define an element to do mass balance

Apply mass balance

$$\overset{o}{Accumulation} * dV = \overset{o}{Flux} |_{in} * A - \overset{o}{Flux} |_{out} * A + \overset{o}{Generation} * dV - \overset{o}{Consumption} * dV$$



Liquid evaporation through a capillary

Solving the evaporation problem in stagnant air

Using average velocity of volumes for convective flux

$$n_1 = j_1^a + c_1 v^a \text{ where } v^a = v^v$$

$$n_1 = -D \frac{dc_1}{dz} + c_1 v^v$$

$$n_1 = -D \frac{dc_1}{dz} + c_1 (\bar{V}_1 n_1)$$

$$D \frac{dc_1}{dz} - c_1 (\bar{V}_1 n_1) + n_1 = 0$$

$$\frac{dc_1}{dz} - \frac{\bar{V}_1 n_1}{D} c_1 + \frac{n_1}{D} = 0$$

$$v^v = c_1 \bar{V}_1 v_1 + c_2 \bar{V}_2 v_2$$

n_1 is constant

$$\bar{V}_1 = \bar{V}_2 = \frac{1}{\bar{c}} \text{ is constant (22.4 liter/mole) in vapor phase at 1 bar.}$$

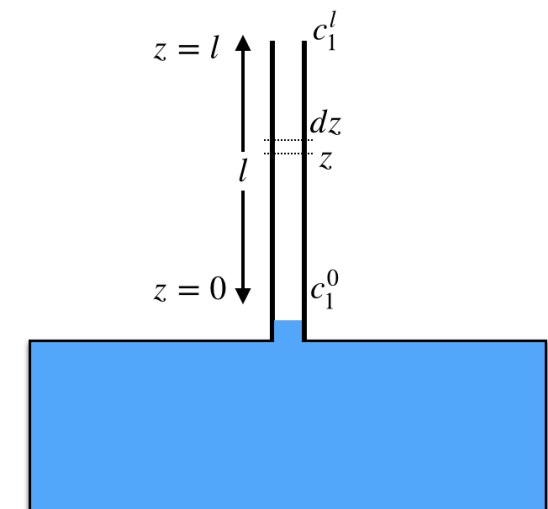
Air is stagnant

$$\Rightarrow v_2 = 0$$

$$\Rightarrow v^v = c_1 \bar{V}_1 v_1 = \bar{V}_1 n_1 \text{ (constant)}$$

Boundary conditions (two boundary conditions for ODE because n_1 is also unknown)

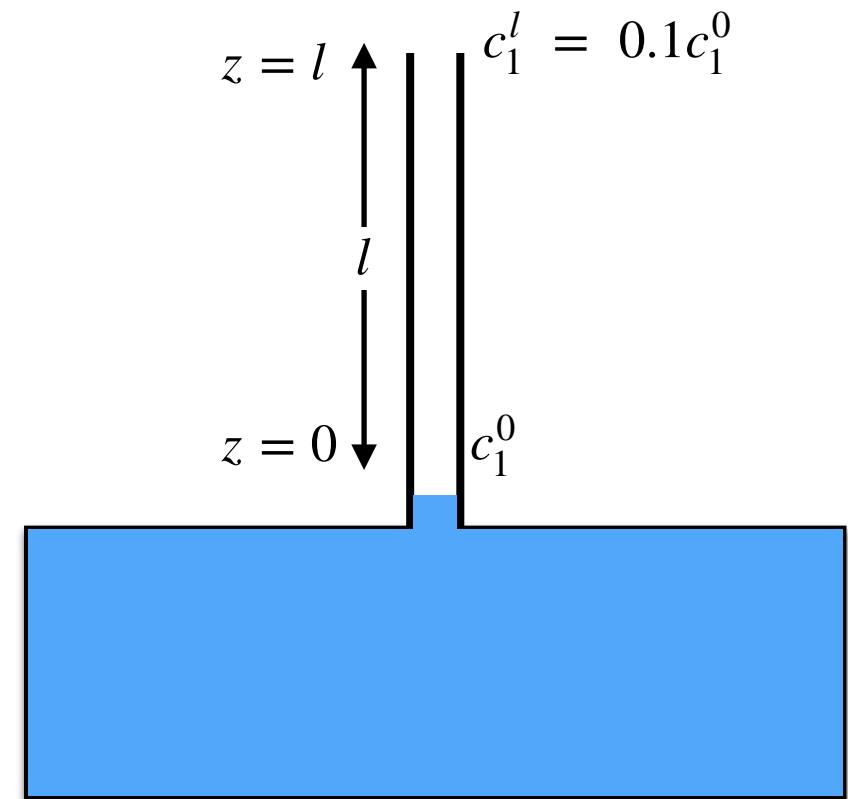
$$\frac{\bar{c} - c_1}{\bar{c} - c_1^0} = \left(\frac{\bar{c} - c_1^l}{\bar{c} - c_1^0} \right)^{\frac{z}{l}} \quad n_1 = \frac{D \bar{c}}{l} \ln \left(\frac{\bar{c} - c_1^l}{\bar{c} - c_1^0} \right)$$



Liquid evaporation through a capillary

Where is the velocity maximum in this case

- A. Top ($z = L$)
- B. Bottom ($z = 0$)
- C. Not enough information
- D. Velocity is constant



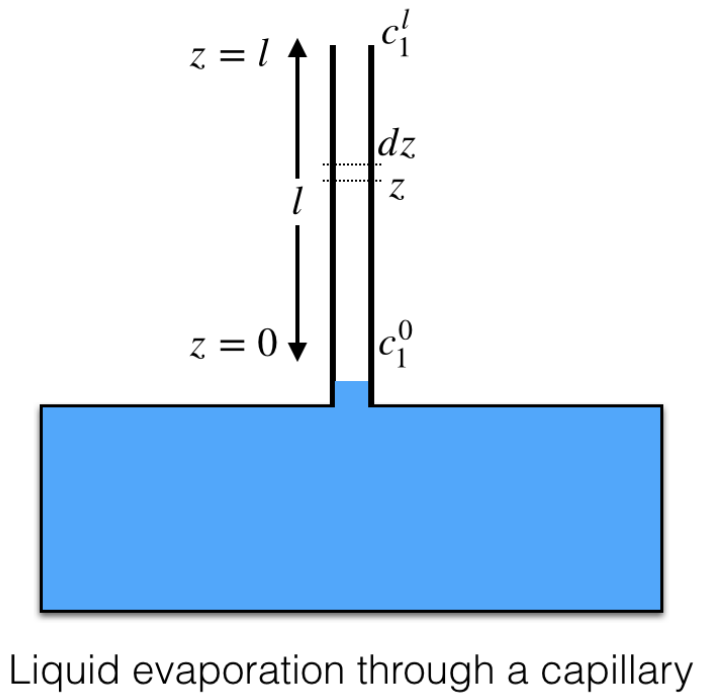
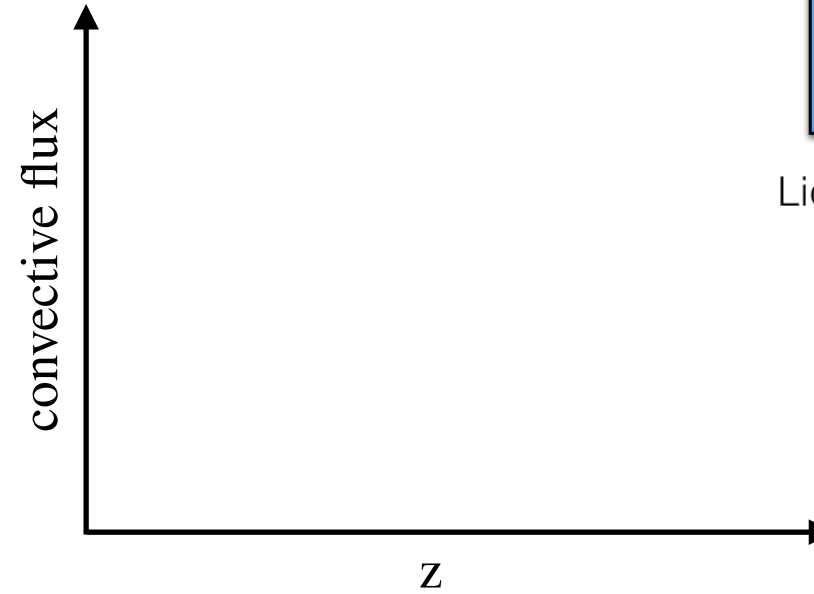
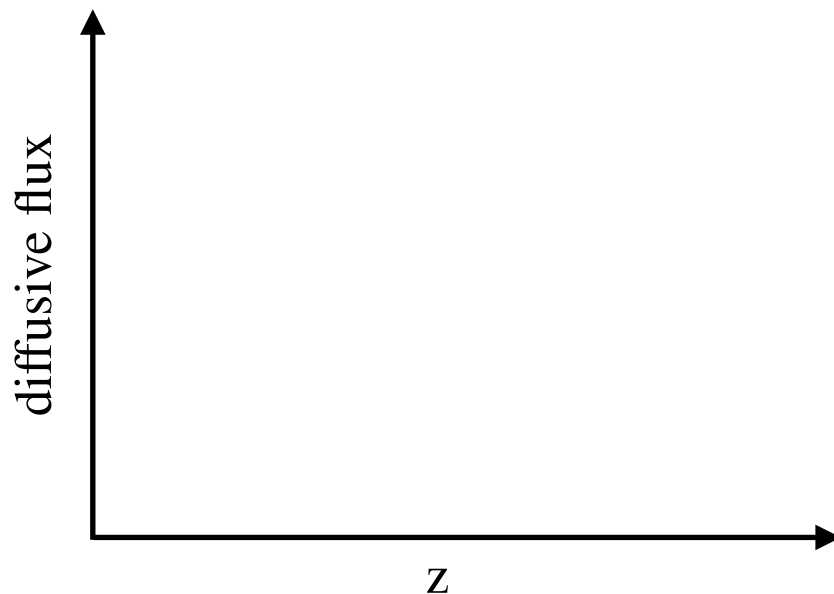
Liquid evaporation through a capillary

Relative contribution of diffusion and convection

$$n_1 = j_1 + c_1 v^v$$

$$n_1 = \frac{D \bar{c}}{l} \ln \left(\frac{\bar{c} - c_1^l}{\bar{c} - c_1^0} \right)$$

$$v^v = c_1 \bar{V}_1 v_1 = \bar{V}_1 n_1 \text{ (constant)}$$

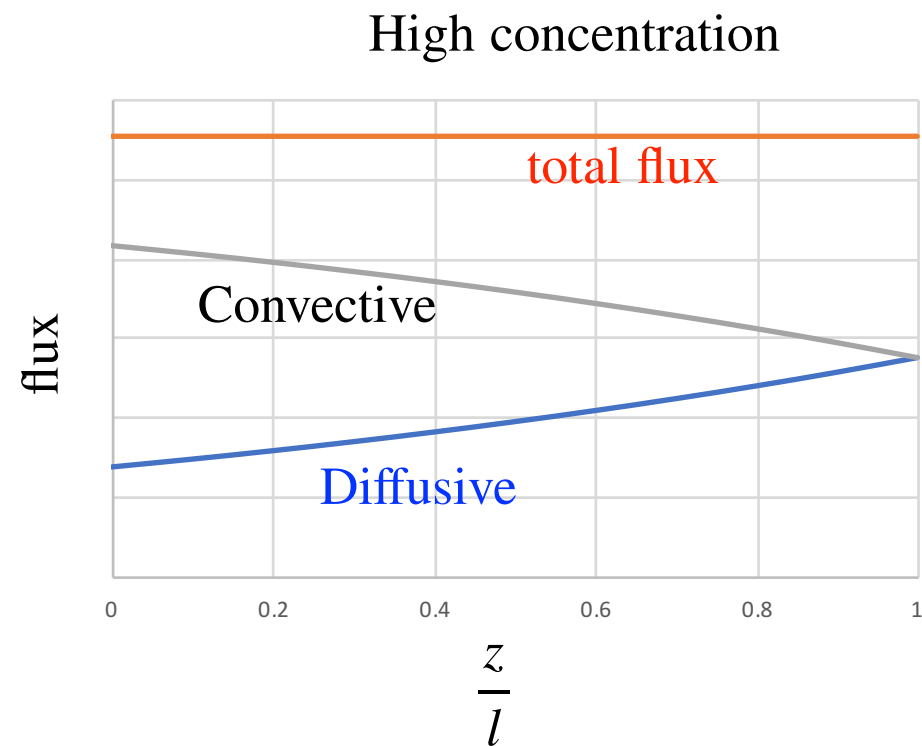
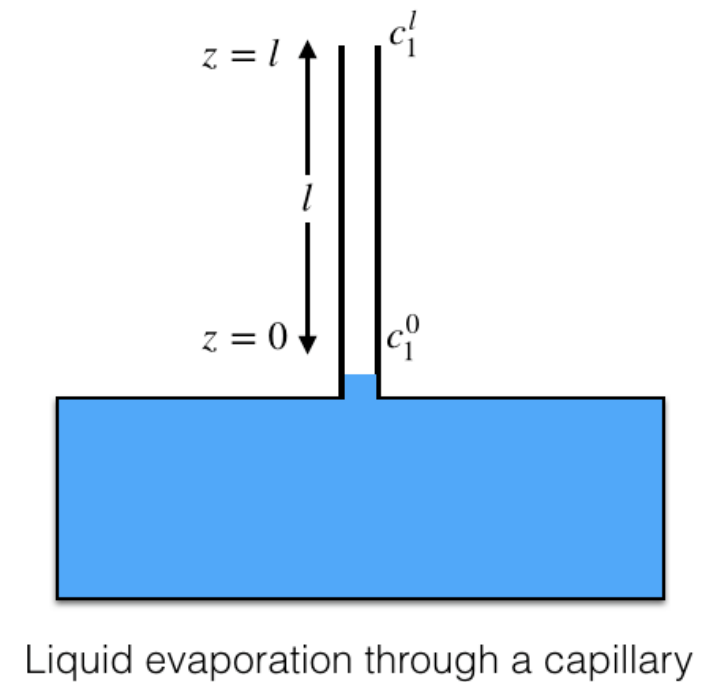
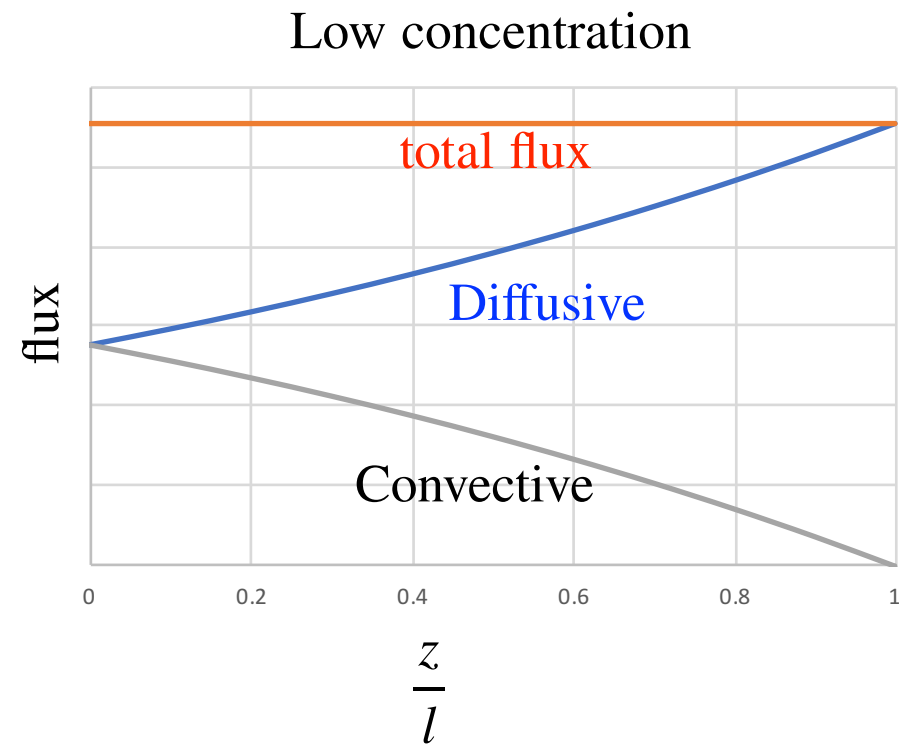


$$n_1 = -D \frac{dc_1}{dz} + c_1 v^v$$

$$v^v = c_1 \bar{V}_1 v_1 = \bar{V}_1 n_1 \text{ (constant)}$$

Convection is higher at higher concentration

Relative contribution of diffusion and convection



Relative contribution of diffusion and convection

$$n_1 = j_1 + c_1 v^v \qquad n_1 = \frac{D \bar{c}}{l} \ln \left(\frac{\bar{c} - c_1^l}{\bar{c} - c_1^0} \right) \qquad \frac{\bar{c} - c_1}{\bar{c} - c_1^0} = \left(\frac{\bar{c} - c_1^l}{\bar{c} - c_1^0} \right)^{\frac{z}{l}}$$

Diffusive part

$$j_1 = -D \frac{dc_1}{dz}$$

Derivative of concentration profile (LHS)

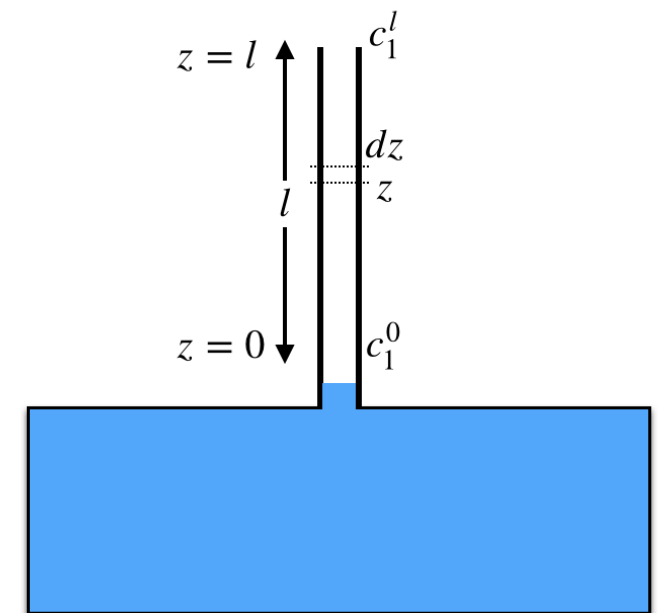
$$\frac{d}{dz} \left(\frac{\bar{c} - c_1}{\bar{c} - c_1^0} \right) = - \left(\frac{1}{\bar{c} - c_1^0} \right) \frac{dc_1}{dz}$$

Derivative of RHS

$$\frac{da^z}{dz} = a^z \ln a$$

$$\frac{d}{dz} \left(\frac{\bar{c} - c_1^l}{\bar{c} - c_1^0} \right)^{\frac{z}{l}} = \frac{1}{l} \left(\frac{\bar{c} - c_1^l}{\bar{c} - c_1^0} \right)^{\frac{z}{l}} \ln \left(\frac{\bar{c} - c_1^l}{\bar{c} - c_1^0} \right)$$

$$j_1 = -D \frac{dc_1}{dz} = \frac{D(\bar{c} - c_1^0)}{l} \left(\frac{\bar{c} - c_1^l}{\bar{c} - c_1^0} \right)^{\frac{z}{l}} \ln \left(\frac{\bar{c} - c_1^l}{\bar{c} - c_1^0} \right)$$



Liquid evaporation through a capillary

Alternatively

Convective flux

$$c_1 v^v = c_1 \bar{V}_1 n_1 = \frac{c_1}{\bar{c}} n_1 \approx y_1 n_1$$

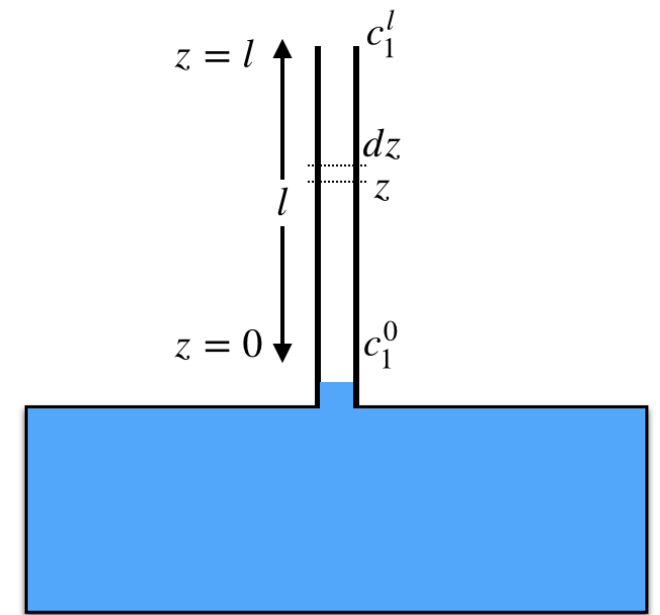
Diffusive flux = Total flux - Convective flux

$$j_1 = n_1 - c_1 v^v = n_1 - \frac{c_1}{\bar{c}} n_1 = n_1 \left(\frac{\bar{c} - c_1}{\bar{c}} \right)$$

$$n_1 = \frac{D \bar{c}}{l} \ln \left(\frac{\bar{c} - c_1^l}{\bar{c} - c_1^0} \right)$$

$$\Rightarrow j_1 = \frac{D \bar{c}}{l} \ln \left(\frac{\bar{c} - c_1^l}{\bar{c} - c_1^0} \right) \left(\frac{\bar{c} - c_1}{\bar{c}} \right) \quad \frac{\bar{c} - c_1}{\bar{c} - c_1^0} = \left(\frac{\bar{c} - c_1^l}{\bar{c} - c_1^0} \right)^{\frac{z}{l}} \longrightarrow (\bar{c} - c_1) = (\bar{c} - c_1^0) \left(\frac{\bar{c} - c_1^l}{\bar{c} - c_1^0} \right)^{\frac{z}{l}}$$

$$\Rightarrow j_1 = \frac{D(\bar{c} - c_1^0)}{l} \left(\frac{\bar{c} - c_1^l}{\bar{c} - c_1^0} \right)^{\frac{z}{l}} \ln \left(\frac{\bar{c} - c_1^l}{\bar{c} - c_1^0} \right)$$



Liquid evaporation through a capillary

Relative contribution of diffusion and convection

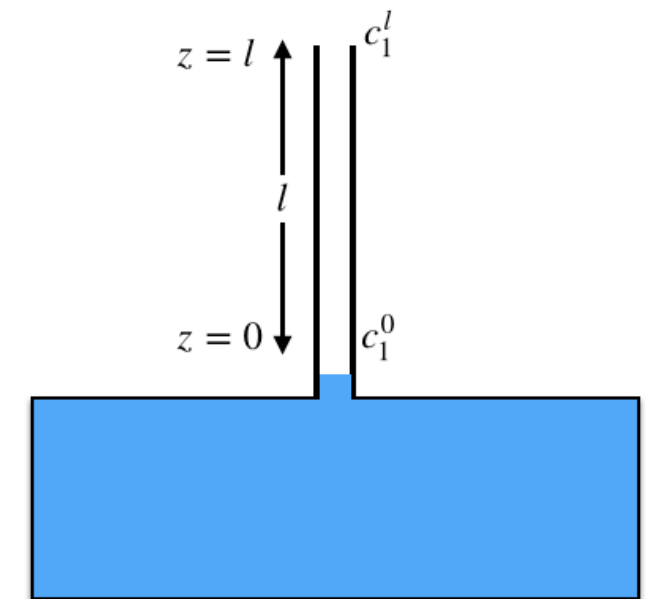
Total flux is constant $n_1 = \frac{D\bar{c}}{l} \ln\left(\frac{\bar{c} - c_1^l}{\bar{c} - c_1^0}\right)$

$$j_1 = \frac{D(\bar{c} - c_1^0)}{l} \left(\frac{\bar{c} - c_1^l}{\bar{c} - c_1^0}\right)^{\frac{z}{l}} \ln\left(\frac{\bar{c} - c_1^l}{\bar{c} - c_1^0}\right)$$

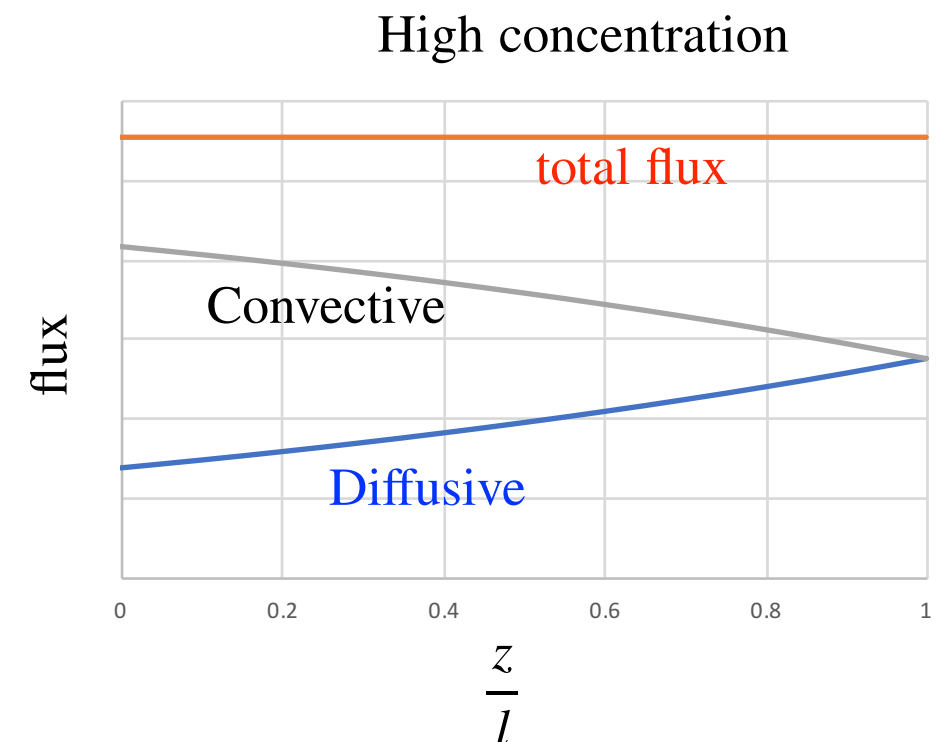
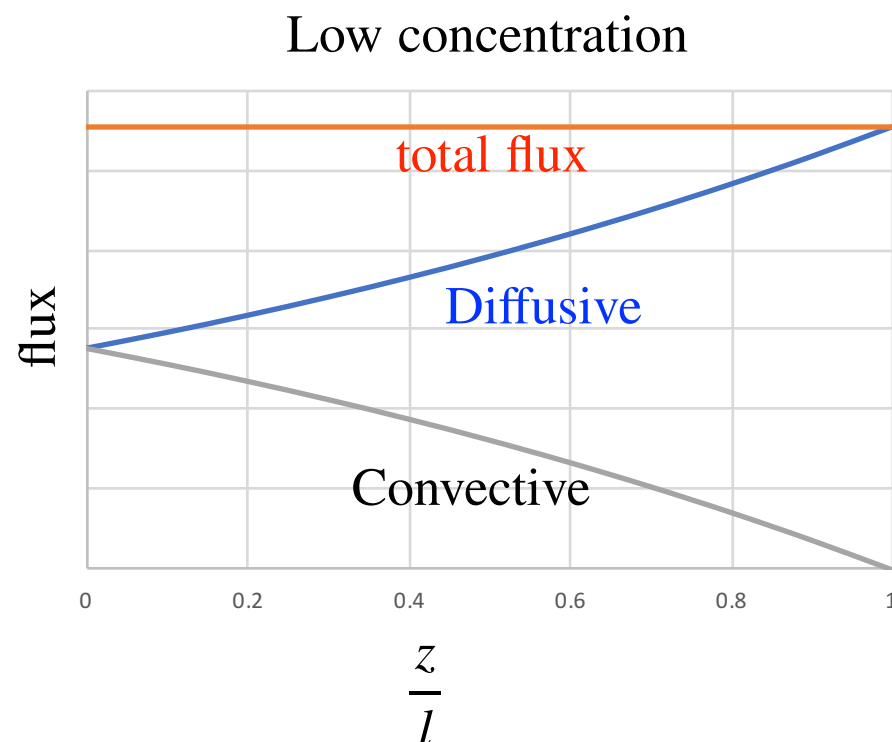
$$\left(\frac{\bar{c} - c_1^l}{\bar{c} - c_1^0}\right) > 1 \Rightarrow \text{Diffusive part is maximum at } z = l$$

Convective part = $n_1 - j_1 = \frac{c_1}{\bar{c}} n_1$ is maximum at $z = 0$

- Higher concentration c_1^0 leads to higher total flux



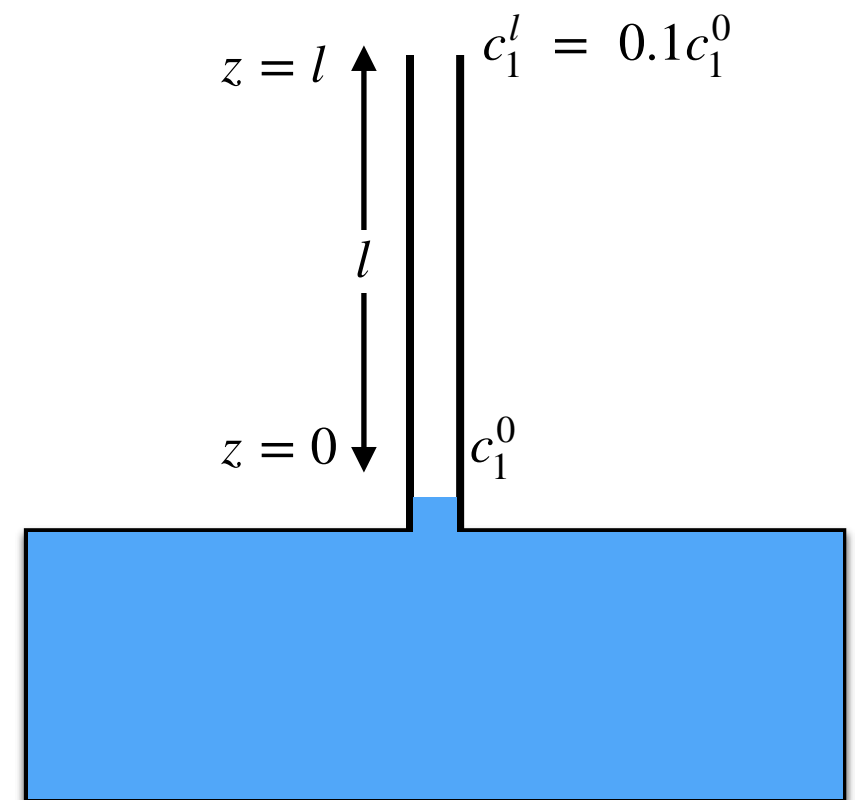
Liquid evaporation through a capillary



In class problem:

Calculate velocity of component 1 at $z = 0$ and $z = l$

$$\begin{aligned} c_1^0 &= 0.02 \text{ mole/liter} & c_1^l &= 0.1c_1^0 \\ D &= 1 \text{ cm}^2 \text{ s}^{-1} & l &= 10 \text{ cm} \end{aligned}$$



Liquid evaporation through a capillary

Consider the following problem with diffusion, convection and reaction at steady-state



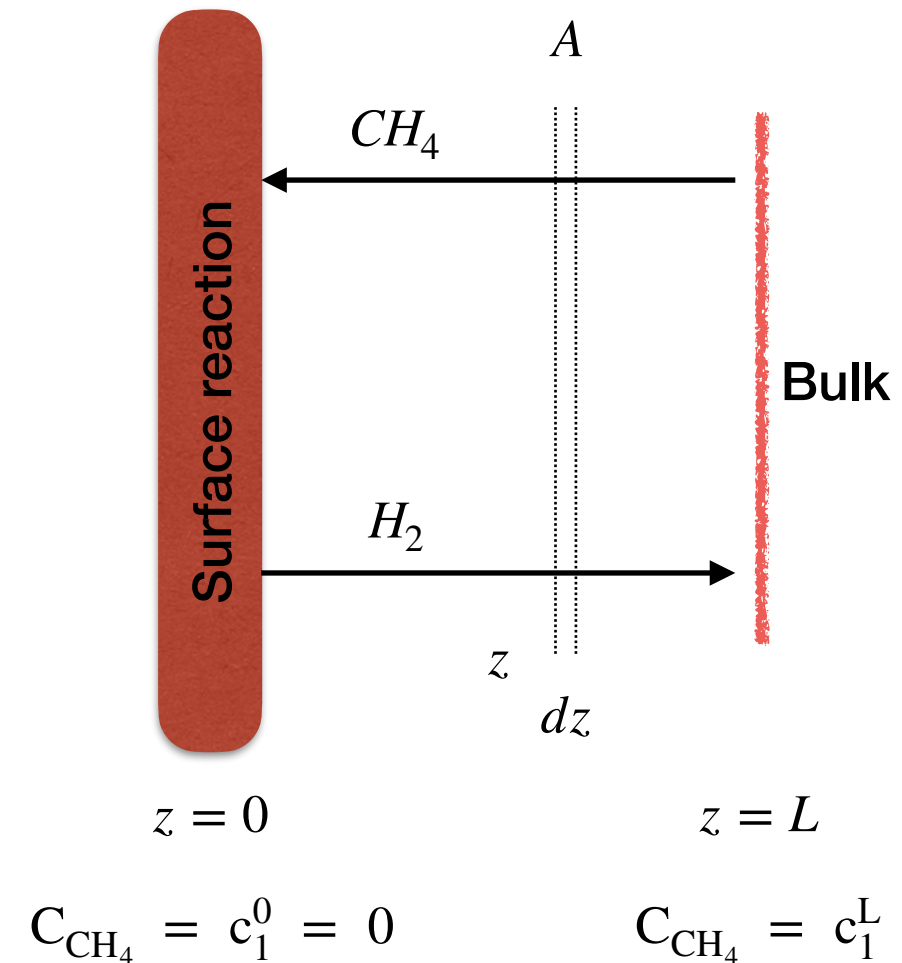
Calculate concentration profile of CH_4

Define your system -

Define an element to do mass balance

Apply mass balance

$$\overset{o}{Accumulation} * dV = \overset{o}{Flux} |_{in} * A - \overset{o}{Flux} |_{out} * A + \overset{o}{Generation} * dV - \overset{o}{Consumption} * dV$$



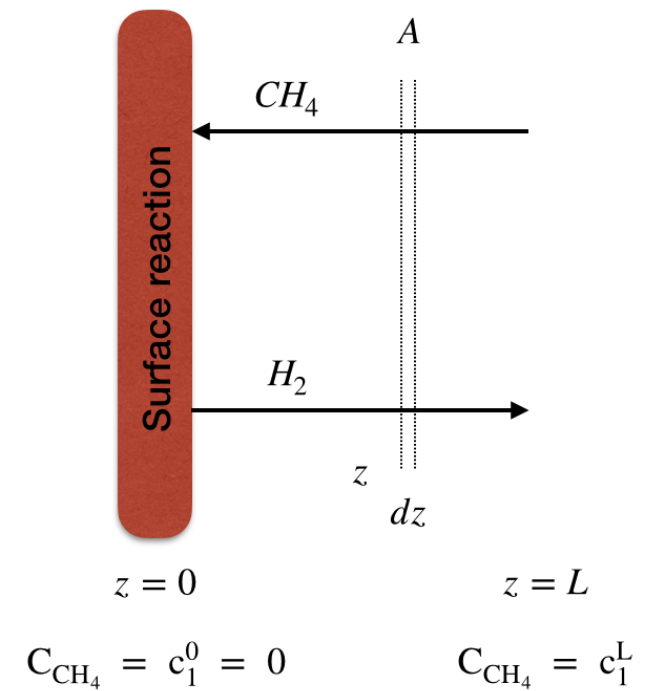
$$\frac{dn_1}{dz} = 0$$

n_1 is constant

Similarly

$$\frac{dn_2}{dz} = 0$$

n_2 is constant



Let's look at the boundary; $z = 0$



$$n_2 = -2n_1$$

$$n = n_1 + n_2 = n_1 - 2n_1 = -n_1$$

We can use mole average velocity because we are dealing with gases

$$v = y_1 v_1 + y_2 v_2$$

$$n_1 = -Dc \nabla y_1 + c_1 v$$

$$n = n_1 + n_2 = cv$$

$$\Rightarrow n_1 = -Dc \nabla y_1 + y_1 cv$$

$$\Rightarrow n_1 = -Dc \nabla y_1 + y_1 n$$

$$n_1(1 + y_1) = -Dc \frac{dy}{dz}$$

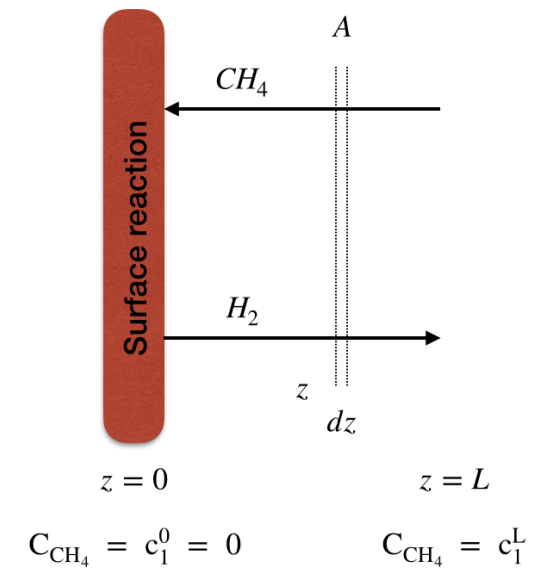
$$\Rightarrow n_1 = -Dc \nabla y_1 - y_1 n_1$$

$$\int_0^z \frac{n_1}{Dc} dz = - \int_0^{y_1} \frac{dy}{(1 + y_1)}$$

$$\text{at } z = 0, C_{\text{CH}_4} = c_1^0 = 0$$

$$\int_0^z \frac{n_1}{Dc} dz = - \int_0^{y_1} \frac{dy}{(1 + y_1)}$$

$$\Rightarrow \frac{n_1 z}{Dc} = - \ln(1 + y_1)$$



at $z = L$, $C_{CH_4} = c_1^L$

$$\Rightarrow \frac{n_1 L}{Dc} = - \ln(1 + y_1^L)$$

$$\Rightarrow n_1 = - \frac{Dc}{L} \ln(1 + y_1^L)$$

$$\Rightarrow \ln(1 + y_1) = - \frac{n_1 z}{Dc} = \frac{z}{L} \ln(1 + y_1^L) = \ln(1 + y_1^L)^{z/L}$$

$$\Rightarrow 1 + y_1 = (1 + y_1^L)^{z/L}$$

$$\Rightarrow y_1 = (1 + y_1^L)^{z/L} - 1$$

Exercise problem #1

Compare total flux when you consider convection and when you neglect convection (use thin film result without convection)

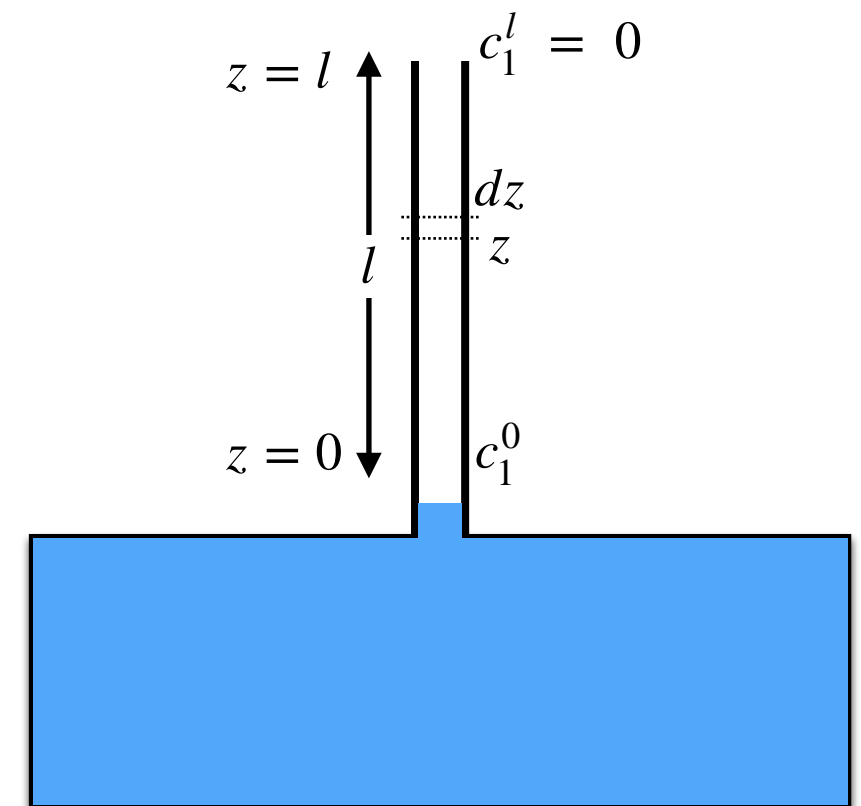
Consider two cases (stagnant air):

Benzene evaporating at 6 °C and 78 °C, Total pressure = 1 atm

$$c_1^l = 0 \quad D = 0.01 \text{ cm}^2/\text{s}; l = 1 \text{ m}$$

$$\bar{c} = \frac{P}{RT} \quad c_1^0 = \frac{P^{sat}}{RT}$$

T (°C)	P ^{sat} (atm)
6	0.049
78	0.934



Liquid evaporation through a capillary

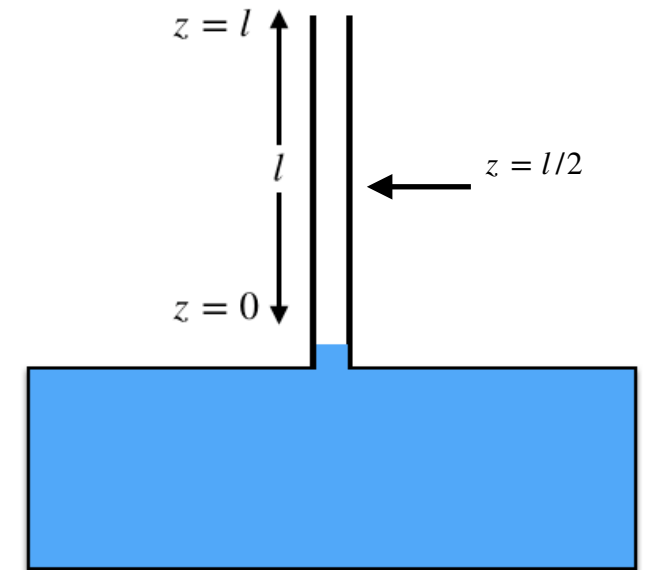
T (°C)	P ^{sat}	$P \ln\left(\frac{P}{P - P^{sat}}\right)$	% Convection
6	0.049		
78	0.934		

Exercise problem #2

We said the air was stagnant, can you calculate the diffusive and convective flux of air?

$$v_2 = 0 \quad \Rightarrow \quad n_2 = c_2 v_2 = 0$$

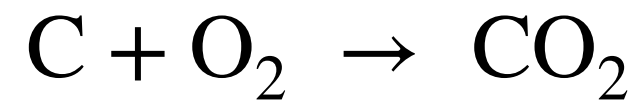
$$n_2 = j_2 + c_2 v^v \quad \Rightarrow \quad j_2 = -c_2 v^v$$



Liquid evaporation through a capillary

Average velocity of volume = v^v

Exercise problem #3



Calculate concentration profile of O_2

Calculate velocity of CO_2 at $z = L$

